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Design of a Glass Tube APH to Increase the Efficiency of the Furnace and Compare with Conventional APH

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Abstract: Air preheater are heat exchanger to preheat or air heating of the combustion air by means of flue gas, steam, water or thermal oil. Air preheaters are used when exhaust temperatures of combustion systems are particularly high. This extracts the hot exhaust valuable energy, which discharged otherwise unused into the atmosphere and warming means of this exhaust heat the combustion air of the combustion process. In the classical use, air preheaters are connected behind high-pressure steam boilers or thermal oil boilers with a flue gas temperature up to 400°C. Their exhaust temperatures lend themselves to preheat the combustion air up to 300 °C. In this way, an air preheater save up to 10% of fuel costs and thus enables payback periods of less than two years. Meanwhile, air preheater also be used in low temperature ranges in order to make the most efficient use of the fuels and counter the rising fuel prices.

Keywords: Air preheaters flue gas temperature, thermal oil, thermal oil boiler, exhaust heat.

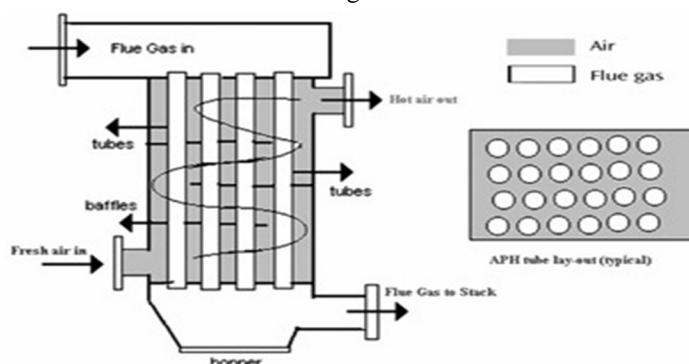
I. INTRODUCTION

Now a day's most of automobile industries having major problem that recovery the failure product to working model. So we analysed some of the methodology that getting New Product Development (NPD) procees by analysing failure cases. For this process we gone through **cross over** failed product by working through design to find error destination to be rectified. We used design software called Auto-Cad for making a rectifying product. Most of industries getting suffered to do production without error and failure of products. But by using this methodology can get clear solution from this and they can improve production as well as reduce cost by making more targets by keeping customer demand in our mind. By analysing failure model we found that major error was degree changing on interlink place of cross over. Finally we changed degree by doing some work flow and specification on failed design to get rectified product.

II. WORK FLOW

- 1) *Step 1:* Prospective studies of the NPD process are performed using the existing literature and preliminary references.
- 2) *Step 2:* Comparative analysis between the current processes and a NPD process is performed.
- 3) *Step 3:* Phase-based evaluations upon failed product cases are conducted with a NPD process so as to identify the abridged steps and root-causes of failures.
- 4) *Step 4:* Finally, renewed priorities are set forth by utilizing the analytic hierarchy process analysis and questionnaire analysis upon the above identified causes of failures.

Diagram



III. OPERATIONS & MAINTENANCE INSTRUCTIONS

A. Equipment Description

The heat exchange surface in the Air Pre-heater consists of Cast iron tubes. The Cast tube air pre-heater module is an assembly of rectangular cast tubes. The cast iron tubes have integral fins on both internal and external surfaces. The entire tube

Assembly is built inside a steel frame made by beams and fully insulated casings.

Air terminal connections are made of rectangular flanges formed from rolled steel sections and forms an integral part of the Air Pre-heater frame. The entire Air Pre-heater assembly can be considered as part of ducting system because of its general arrangement. The tube is made up of two half sections, cast independently and then bolted together. To prevent air leakage the longitudinal direction two grooves have been provided on the flanges on either side. The Air Pre-heater is assembled in 4 super imposed air passes with the axis of the tubes horizontal. Flue gas enters at the top of module no 1 and flows vertically down over the outside of Cast Tubes in series and leaves the Air Pre-heater at the bottom of module No 4 of Air Pre-heater. A static wash water system is installed above the top row of cast tubes.

B. Maintenance

Due to tubular construction of the Cast Air Pre-heater there are extensive flat surfaces nor small ducts nor no flow zones. The whole heat transfer surface is swept by the flue gases thus preventing soot deposit. The Air Pre-heater is to be kept as close as possible to the design conditions and the minimum metal temperature be kept at least 100°C above the flue gas dew point. The Frequency of washing at the beginning of the Air Pre-heater's operation shall be of once in three weeks. This frequency can be decreased provided following conditions are met: The deposits on the cast tube surfaces are not significant. This can be deduced if the PH factor of the outgoing water rises very quickly during the washing procedure. The specified process operating conditions can be achieved. Flue gas pressure drop does not increase drastically and limits ID fan capacity. In case the above conditions cannot be achieved, it is required to wash the Air Pre-heater immediately. The actual frequency of washing of cast tubes may be finalized based on the operational feedback.

IV. DESIGN CALCULATION

PROPERTY	AIR	FLUE GAS
DENSITY	0.74 Kg/m	0.525 Kg/m
VISCOSITY	25.99 N/M	31.68*10 ⁻⁶
THERMAL CONDUCTIVITY	0.03931 N/M.K	0.03260
SPECIFIC HEAT	1.026 KJ/KG K	1.151 KJ/KG K
$\Delta P_{ALLOWABLE}$	110mm H ₂ O	

$$\begin{aligned}
 Q_{lh} &= m_h C_{ph} (T_1 - T_2) \\
 &= 1.2 * 20.53 (383 - 201.2) \\
 Q_{lh} &= Q_{la} \\
 Q_{lc} &= m_c C_{pc} (t_1 - t_2) \\
 t_2 &= t_1 + Q / (m_c C_{pc}) \\
 &= 40 + 45428.0295 / (19.53 * 1.005) \\
 &= 270.69^\circ\text{C}
 \end{aligned}$$

A. For Counter Flow

$$\begin{aligned}
 LMTD &= (T_2 - t_2) - (T_1 - t_1) / [(T_1 - t_2) / (t_2 - t_1) + (T_2 - t_1) / (T_1 - t_1)] \\
 &= 46.89 / 0.343 \\
 &= 136.7^\circ\text{C} \\
 \text{ASSUME} \\
 U_D &= 25 \text{ W/m}^2\text{K} \\
 &= 4528.096 / (25 * 136.8) \\
 A &= 1.32 \text{ m}^2 \\
 A &= 3.14 * d_o L N_T \\
 1.32 &= 1.34 * (19.05 * 10^{-3}) * 7 * N_T \\
 N_T &= 3.15
 \end{aligned}$$

= 4 TUBES

Mass velocity $G_s / A_s = M_s$

$$= 19.53 / 2.73$$

$$= 7.590 \text{ I}_g / \text{ms}^2$$

B. Equivelent D_e For Square Pitch

$$D_e = 1.27 / d_0 (P_r - 0.785 d_0^2)$$

$$= 1.27 / 19.05 * 10^{-3} (25 * 10^{-3} - 0.785 (19.05 * 10^{-3}))$$

$$= 0.03931$$

$$d_e = 0.023 \text{ m}$$

$$N_{RE} = 3.36$$

$$N_{pr} = 25$$

$$= h_0 d_e = 0.36 * (3.36)^{0.55} (25.5)^{0.55}$$

$$= 0.03931$$

$$= 0.8025$$

C. Overall Heat Transfer Coefficient

$$1/U = 1/H_1 + 1/H_2$$

For cast iron aph

$$U = 1.246 \text{ W}/(\text{m}^2 \text{ } ^\circ\text{C})$$

For glass iron aph

$$U = 6.716 \text{ W}/(\text{m}^2 \text{ } ^\circ\text{C})$$

V. CONCLUSIONS

The Objective of the Project is to analyse the efficiency of the AIR PREHEATER and Contrast it with existing convrntional cast iron air preheater. Thus The tabulated results show thst there is a significant increase in the Products efficiency in glass tube air preheater. Thus the project has been elucidated and explained

VI. ACKNOWLEDGMENT

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